

FORM PTO-1390 (Modified)  
(REV 11-98)

U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE

ATTORNEY'S DOCKET NUMBER

TRANSMITTAL LETTER TO THE UNITED STATES  
DESIGNATED/ELECTED OFFICE (DO/EO/US)  
CONCERNING A FILING UNDER 35 U.S.C. 371

PQC-199US

U.S. APPLICATION NO. (IF KNOWN, SEE 37 CFR

Not Yet Assigned **09/700475**INTERNATIONAL APPLICATION NO.  
PCT/US98/10070INTERNATIONAL FILING DATE  
15 May 1998 (15.05.98)PRIORITY DATE CLAIMED  
None

TITLE OF INVENTION

**PEROXIDE, OXYGEN, AND PEROXIDE/OXYGEN BRIGHTENING OF CHEMICAL AND MIXED WASTE PULPS**

APPLICANT(S) FOR DO/EO/US

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FRANCIS, Raymond C.


Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

1. ☒ This is a **FIRST** submission of items concerning a filing under 35 U.S.C. 371.
2. ☐ This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 U.S.C. 371.
3. ☒ This is an express request to begin national examination procedures (35 U.S.C. 371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. 371(b) and PCT Articles 22 and 39(1).
4. ☒ A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
5. ☒ A copy of the International Application as filed (35 U.S.C. 371 (c) (2))
  - a. ☒ is transmitted herewith (required only if not transmitted by the International Bureau).
  - b. ☐ has been transmitted by the International Bureau.
  - c. ☐ is not required, as the application was filed in the United States Receiving Office (RO/US).
6. ☐ A translation of the International Application into English (35 U.S.C. 371(c)(2)).
7. ☒ A copy of the International Search Report (PCT/ISA/210).
8. ☒ Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371 (c)(3))
  - a. ☐ are transmitted herewith (required only if not transmitted by the International Bureau).
  - b. ☐ have been transmitted by the International Bureau.
  - c. ☐ have not been made; however, the time limit for making such amendments has NOT expired.
  - d. ☒ have not been made and will not be made.
9. ☐ A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).
10. ☒ An oath or declaration of the inventor(s) (35 U.S.C. 371 (c)(4)) (Unexecuted).
11. ☒ A copy of the International Preliminary Examination Report (PCT/IPEA/409) dated 18 August 2000.
12. ☐ A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371 (c)(5)).

## Items 13 to 20 below concern document(s) or information included:

13. ☐ An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
14. ☐ An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
15. ☐ A **FIRST** preliminary amendment.
16. ☐ A **SECOND** or **SUBSEQUENT** preliminary amendment.
17. ☐ A substitute specification.
18. ☐ A change of power of attorney and/or address letter.
19. ☒ Certificate of Mailing by Express Mail
20. ☒ Other items or information:

Second IPE Report (PCT/IPEA/409) dated 29 August 2000 with amended claims attached.

U.S. APPLICATION NO. (IF KNOWN, SEE 37 CFR 1.53) Not Yet Assigned		INTERNATIONAL APPLICATION NO. PCT/US98/10070		ATTORNEY'S DOCKET NUMBER PQC-199US	
21. The following fees are submitted:				CALCULATIONS PTO USE ONLY	
<b>BASIC NATIONAL FEE ( 37 CFR 1.492 (a) (1) - (5)) :</b>					
<input type="checkbox"/> Neither international preliminary examination fee (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO and International Search Report not prepared by the EPO or JPO . . . . . \$970.00					
<input checked="" type="checkbox"/> International preliminary examination fee (37 CFR 1.482) not paid to USPTO but International Search Report prepared by the EPO or JPO . . . . . \$860.00					
<input type="checkbox"/> International preliminary examination fee (37 CFR 1.482) not paid to USPTO but international search fee (37 CFR 1.445(a)(2)) paid to USPTO . . . . . \$690.00					
<input type="checkbox"/> International preliminary examination fee paid to USPTO (37 CFR 1.482) but all claims did not satisfy provisions of PCT Article 33(1)-(4) . . . . . \$670.00					
<input type="checkbox"/> International preliminary examination fee paid to USPTO (37 CFR 1.482) and all claims satisfied provisions of PCT Article 33(1)-(4) . . . . . \$96.00					
<b>ENTER APPROPRIATE BASIC FEE AMOUNT =</b>				<b>\$860.00</b>	
Surcharge of \$130.00 for furnishing the oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492 (e)).				<b>\$0.00</b>	
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE		
Total claims	24 - 20 =	4	x \$18.00	<b>\$72.00</b>	
Independent claims	5 - 3 =	2	x \$80.00	<b>\$160.00</b>	
Multiple Dependent Claims (check if applicable).			<input type="checkbox"/>	<b>\$0.00</b>	
<b>TOTAL OF ABOVE CALCULATIONS =</b>				<b>\$1,092.00</b>	
Reduction of 1/2 for filing by small entity, if applicable. Verified Small Entity Statement must also be filed (Note 37 CFR 1.9, 1.27, 1.28) (check if applicable).				<input type="checkbox"/> <b>\$0.00</b>	
<b>SUBTOTAL =</b>				<b>\$1,092.00</b>	
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492 (f)).				<b>\$0.00</b>	
<b>TOTAL NATIONAL FEE =</b>				<b>\$1,092.00</b>	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31) (check if applicable).				<input type="checkbox"/> <b>\$0.00</b>	
<b>TOTAL FEES ENCLOSED =</b>				<b>\$1,092.00</b>	
				Amount to be:	\$
				refunded	
				charged	\$
<input checked="" type="checkbox"/> A check in the amount of <b>\$1,092.00</b> to cover the above fees is enclosed.					
<input type="checkbox"/> Please charge my Deposit Account No. _____ in the amount of _____ to cover the above fees. A duplicate copy of this sheet is enclosed.					
<input checked="" type="checkbox"/> The Commissioner is hereby authorized to charge any fees which may be required, or credit any overpayment to Deposit Account No. <b>18-0350</b> A duplicate copy of this sheet is enclosed.					
<b>NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed and granted to restore the application to pending status.</b>					
SEND ALL CORRESPONDENCE TO:					
<div>Christopher R. Lewis RATNER &amp; PRESTIA Suite 301 One Westlakes (Berwyn) P.O. Box 980 Valley Forge, PA 19482-0980  Phone: (610) 407-0700 Facsimile: (610) 407-0701</div> <div> SIGNATURE  Christopher R. Lewis NAME  36,201 REGISTRATION NUMBER  November 15, 2000 DATE</div>					

PEROXIDE, OXYGEN, AND PEROXIDE/OXYGEN BRIGHTENING  
OF CHEMICAL AND MIXED WASTE PULPS

FIELD OF THE INVENTION

5 The present invention pertains to the brightening of chemical pulps and deinked, mixed office waste pulps, and particularly to the brightening of such pulps in a peroxide or peroxide/oxygen stage of brightening.

BACKGROUND OF THE INVENTION

10 The process of making paper from wood involves the following general stages: (1) bark removal; (2) wood chipping; (3) pulping; (4) brightening; and (5) forming a sheet of paper on a machine. During pulping, wood is reduced to its fibrous state, with a portion of the lignin content in the wood being removed. Pulp can be divided into two main categories - chemical and mechanical pulps - depending on how they are made from wood. Chemical pulping involves the use of chemical reagents to effect a separation of the cellulose fibers from the other wood components, such as lignin and other extraneous compounds. In the process, most of the hemicelluloses are also dissolved. Thus, 15 the yield for chemical pulping is typically 40-50% on wood.

20 Mechanical pulping involves the reduction of wood to the fibrous state by mechanical means, such as by grinding logs into pulp by large revolving grindstones. These pulps are called "mechanical" because a significant amount of mechanical energy (grinding or refining) is required to break down the wood chips. Except for a few water soluble components, all of the constituents of the wood are present in the ground wood pulp. Thus, mechanical pulps are characterized by their high yield and high lignin content. For example, although chemical pulps contain only about 5% lignin (weight basis on pulp) after pulping, 25 mechanical pulps typically contain greater than 20% lignin for hardwoods and 25% for softwoods after pulping.

In general, the brightening of chemical and mechanical pulps occur by different mechanisms. This difference in approach is due, in part, to the difference in lignin content between the chemical and mechanical pulps and to the

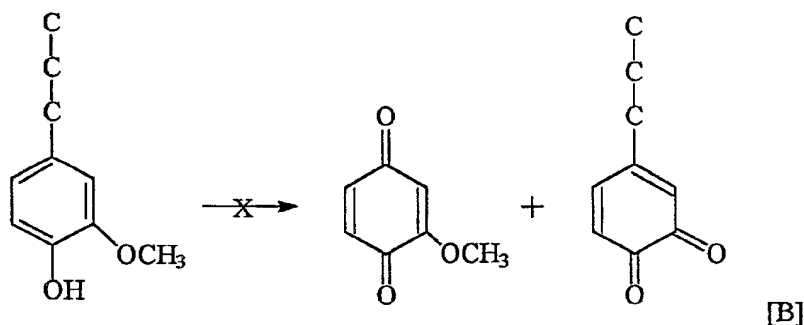
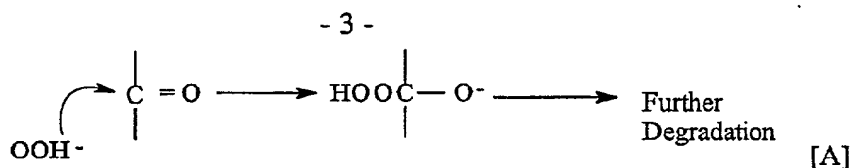
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different nature of the lignin in chemical pulps than that in mechanical pulps. The remaining lignin in chemical pulps is typically more difficult to degrade than the majority of the lignin remaining in mechanical pulps. For example, chemical pulps, such as kraft pulps, are more difficult to brighten by  $H_2O_2$ . Thus, instead of the 60°C bleaching temperature used for mechanical pulps, values in the range of 110°C are used for kraft pulps (which use sodium hydroxide and sodium sulfide as the primary chemical reagents). As another example of the differences in brightening the two different types of pulp, chlorine dioxide ( $ClO_2$ ), a stable free radical, is involved in the brightening of more than 90% of bleached kraft pulp produced in the U.S.A. per year. On the other hand, it has been reported that chlorine dioxide actually darkens mechanical pulps. In sum, results obtained with mechanical pulps cannot be considered as being predictive for chemical pulps.

Various additives have been proposed to improve the brightening process of mechanical pulps or mixed chemical/mechanical pulps having a high lignin content (i.e., above 20% by weight on pulp). Sodium silicate is widely used for hydrogen peroxide brightening of such pulps. It acts as a peroxide stabilizer and as a buffer during the bleaching reaction. Sodium silicate, in combination with a small dose of  $MgSO_4$ , has long been known to improve the brightness of mechanical pulps. The two chemicals are known to form an intermediate that adsorbs or complexes transition metal species which would otherwise undesirably catalyze the decomposition of  $H_2O_2$ . The two chemical combination is widely used in installations that bleach mechanical pulps. When magnesium sulfate has been used for such pulps, however, no increase in brightness has been observed when the  $MgSO_4 \cdot 7H_2O$  dose is increased above 0.05% on mechanical pulp (2.0 mmoles/kg). Accordingly, previous researchers had no need to add more magnesium to their pulps.

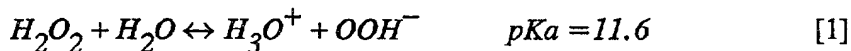
Turning to the brightening of chemical pulps, some results have suggested that silicate has a negative effect on  $H_2O_2$  bleaching of kraft pulps. In some cases, the inclusion of silicate lowered the brightness by 4.6 percentage points (measured as % GE brightness in accordance with TAPPI Standard T452 om-92) and by 2-7 percentage points.

In peroxide brightening of mechanical pulps, the key is nucleophilic degradation of carbonyl compounds in the native lignin without the oxidation of phenols to o- and p- quinones, as shown below in reactions [A] and [B], respectively.

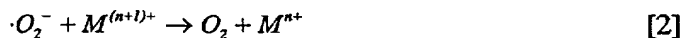


Reaction [A] is the desirable degradation of carbonyl compounds by the perhydroxyl anion,  $\text{OOH}^-$ . This reaction breaks down the carbonyl compounds, which absorb light in the visible range, to a more soluble form to be washed away by water. On the other hand, reaction [B] represents the undesirable formation of o- and p- quinones, which are less soluble in water and also absorb light in the visible range.

The perhydroxyl anion is generated by the dissociation of  $\text{H}_2\text{O}_2$  as shown by equation [1] below. Mild conditions have to be used to prevent the oxidation of phenolics.



Mechanical pulps contain high concentrations of lignin and extractives whose negatively charged sites may complex transition metals. Also, some transition metal catalysis can be tolerated because lignin is a very good radical scavenger. It will scavenge the superoxide anion ( $\cdot\text{O}_2^-$ ) and prevent wasteful decomposition to  $\text{O}_2$  (equation [2]).

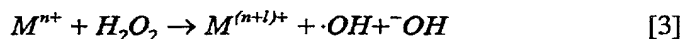


Actually,  $\cdot\text{O}_2^-$  is nucleophilic and its reaction with lignin is reported to result in increased brightness. In sum, transition metal deactivation by magnesium silicates is important but not critical to the brightening of mechanical pulps.

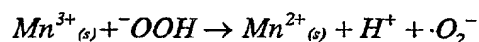
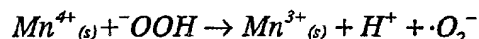
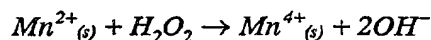
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Unlike softwood mechanical pulps which typically contain about 25 % lignin (by weight on pulp), chemical pulps enter the final brightening stage with typically less than 2 % lignin, which is typically colored and very difficult to oxidize. The approach with  $H_2O_2$  is nucleophilic degradation by  $OOH^-$ .

- 5 However, equation [2] becomes favorable because there is not a large amount of reactive lignin to scavenge  $\cdot O_2^-$ . Equation [2], in conjunction with equations [3] and [4], results in wasteful decomposition of  $H_2O_2$ .

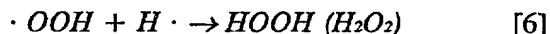


- 10 Equation [3] is favorable for Cu(I) and Fe(II) but not for Mn(II). A more probable mechanism for Mn(II) is outlined below. The subscripted s indicates soluble Mn(IV) and Mn(III).



- 15 Lignin degradation by  $OOH^-$  requires a high temperature because of the unreactive nature of the lignin in chemical pulps. At 110°C, transition metal deactivation is extremely important.

With respect to  $O_2$  delignification, a simple and well-accepted scheme for free radical generation is provided below. RH is a reactive structure in the solution phase.



(Abstraction of H atom from lignin)



- 25  $H_2O_2$  and ROOH will be affected by transition metals in the same manner as in a peroxide/oxygen stage. Thus, the oxygen stage is similar to the peroxide/oxygen stage in that they both involve heterolytic (i.e., ionic) reactions and homolytic (i.e., free radical) reactions. In addition, they are both similar in that both rely on

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hydrogen peroxide, either as added in the peroxide/oxygen stage or as generated in reaction [6] above in the oxygen stage, to perform a brightening function. It is assumed that organic peroxides (ROOH in equation [8]) generated during oxygen delignification dissociate to form  $\text{ROO}^\cdot$  nucleophiles that brighten lignin.

5 Accordingly, in both stages (as well as in a peroxide stage), one must be concerned about transition metals undesirably catalyzing free radical reactions.

### SUMMARY OF THE INVENTION

The present invention provides a combination of additives and methods for brightening pulps containing less than 18% lignin. The invention can  
10 be used in either the peroxide, oxygen, or peroxide/oxygen brightening stages. The additives according to the present invention include an aqueous sodium silicate solution, an alkali agent, and a magnesium compound which dissociates in the solution to form  $\text{Mg}(\text{OH})^+$  cations. The alkali agent is added in an amount sufficient to maintain a pH of at least about 8, and the magnesium compound is  
15 added in an amount to achieve, along with any other dissociated magnesium, an  $\text{Mg}:\text{SiO}_2$  mass ratio of between about 1:46 to about 1:2.

A method for brightening pulp according to the present invention involves mixing pulp containing less than 18% lignin with an aqueous sodium silicate solution, an alkali agent, and a magnesium compound which dissociates in  
20 the solution to form  $\text{Mg}(\text{OH})^+$  cations. The alkali agent and magnesium compound are added to achieve the same pH range and weight ratio mentioned above. The method also includes heating the mixture to allow the mixture to react to cause a portion of the lignin in the pulp to degrade.

According to another embodiment of the present invention directed  
25 to the peroxide or peroxide/oxygen brightening stages, a method for brightening pulp containing transition metals, hydrogen peroxide, and less than 18% lignin includes first forming a sodium silicate mixture having a high percentage of high molecular weight silicates. This is accomplished by mixing sodium silicate and a magnesium compound which dissociates in the solution to form  $\text{Mg}(\text{OH})^+$  cations.  
30 This sodium silicate mixture is then added to the pulp to adsorb at least a portion of the transition metals.

The present invention also includes an aqueous composition for use in brightening pulps. The composition includes pulp containing less than 18% lignin, an aqueous sodium silicate solution, an alkali agent, and a magnesium  
35 compound which dissociates in the solution to form  $\text{Mg}(\text{OH})^+$  cations. The alkali

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agent and magnesium compound are added to achieve the same pH range and weight ratio mentioned above.

It is to be understood that both the foregoing general description and the following detailed description are exemplary, but are not restrictive, of the invention.

#### DETAILED DESCRIPTION OF THE INVENTION

The present invention is directed to the brightening of certain pulps during peroxide, oxygen, or peroxide/oxygen brightening. As used herein, the term "brightening stage" shall mean either a peroxide stage, an oxygen stage, or a peroxide/oxygen stage. The typical operating conditions and conventional additives to these stages are well known. During such brightening, hydrogen peroxide serves to degrade carbonyl groups of lignin, rendering them more water soluble. In the absence of such degradation, lignin would remain in the pulp, causing the brightness of the pulp to remain lower than would be if such lignin were removed. Transition metals present in the pulp undesirably react with hydrogen peroxide thereby precluding hydrogen peroxide from serving its function of degrading lignin. The present invention is based in part on the recognition that higher molecular weight silicates assist in adsorbing transition metals thus preventing them from undesirably reacting with hydrogen peroxide. The present invention is also based on the recognition that  $\text{Mg}(\text{OH})^+$  plays a significant role in the molecular weight distribution of a sodium silicate solution. More particularly, the presence of  $\text{Mg}(\text{OH})^+$  in a sodium silicate solution, over a certain  $\text{Mg}:\text{SiO}_2$  mass ratio, enhances the formation of higher molecular weight silicates.

Accordingly, the present invention is directed to various compositions and methods embodying this concept. The invention provides a combination of additives (either to hydrogen peroxide, oxygen, or a combination thereof, depending on which one of the three brightening stages is being employed) for brightening pulps containing less than 18% lignin. In this case, these additives include an aqueous sodium silicate solution, an alkali agent, and a magnesium compound which dissociates in the solution to form  $\text{Mg}(\text{OH})^+$  cations. The invention also encompasses an aqueous composition for use in brightening pulps comprising pulp containing less than 18% lignin, hydrogen peroxide (either as an additive or as reacted from reaction [6] above), an aqueous sodium silicate solution, an alkali agent, and a magnesium compound which dissociates in the



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solution to form  $\text{Mg}(\text{OH})^+$  cations. The present invention also provides a method for brightening pulp including forming a mixture of the pulp, hydrogen peroxide, aqueous sodium silicate solution, alkali agent, and magnesium compound, then heating the mixture to allow it to react to cause a portion of the lignin to degrade. Finally, the invention is characterized as a method for brightening pulp containing transition metals and less than 18% lignin. This method includes the steps of forming a sodium silicate mixture having a high percentage of high molecular weight silicates by mixing sodium silicate and a suitable magnesium compound, and adding the sodium silicate mixture to the pulp.

The pulp used in connection with the present invention is defined broadly as any pulp having less than 18% lignin (on pulp). Unless otherwise specified, all percentages of lignin include all forms of lignin and are given as weight percentages of the total pulp, on a dry weight basis, so that 18% lignin means that there are 18 grams of lignin in a 100 gram sample of pulp (excluding the weight of water).

Stated another way, the invention can be used with any pulp in which more than 50% of the lignin (by weight, on wood) is removed during pulping. This means that more than half of the original lignin present in the wood is removed during the pulping process. For softwoods, having an average lignin content of 28.6% (by weight, on wood), the removal of half of the original lignin content of the wood during a conventional chemical pulping process results in a pulp having 23.3% lignin (on pulp). For hardwoods, having an average lignin content of 24.1% (by weight, on wood), the removal of half of the original lignin content of the wood during a conventional chemical pulping process results in a pulp having 18.0% lignin (on pulp). The development of these final lignin contents factors in the yield from conventional chemical pulping processes. Thus, any pulp with less than 18% lignin (on pulp) would typically include at least some pulp which was processed by chemical pulping or was derived from a wood having a relatively low initial content of lignin.

In general, chemical pulping processes are continued until the lignin content is reduced to about 5% (on pulp) or less. It is preferable to use the present invention to brighten such pulps. In addition, chemical pulps typically undergo further delignification before the final brightening stage (i.e., peroxide or peroxide/oxygen) such that the pulps contain about 1-2% lignin before the final brightening stage. Pulps brightened by the present invention can also include such pulps which have been further delignified. The present invention can also be used

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to brighten pulps having recycled pulps, in which chemical and mechanical pulps are mixed, as long as the average lignin content is less than about 18%. Pulps brightened by the present invention also include semichemical pulps with lignin content varying from approximately 10 to 18%. In Example 4 below, bleached and unbleached samples of de-inked mixed office waste consisting of 65% sorted white ledger and 35% office pack were obtained from a mill in the American Midwest.

The additives of the present invention are used in the peroxide, oxygen, or peroxide/oxygen stages of brightening. The process parameters of these stages are well known. For example, a typical charge of peroxide loading is 20 kg of hydrogen peroxide per metric ton of pulp. The hydrogen peroxide is mixed while the mixture is heated, typically to a temperature of between about 90°C to about 130°C, often 110°C. Water is also added, typically to achieve a consistency of about 15% solids. Of course, reaction time, temperature, and consistency are all interrelated and can be varied in a known manner. A hydrogen peroxide/oxygen stage is similar to a hydrogen peroxide stage except that the slurry is pressurized with oxygen.

An oxygen stage is similar to a hydrogen peroxide/oxygen stage except that no hydrogen peroxide is added. Oxygen delignification is also conducted over a wider consistency range (10% to 35% solids) but 12% to 15% solids is typical. In general, an oxygen stage does not brighten as well as a peroxide stage or as a peroxide/oxygen stage. Oxygen or an oxygen-containing gas (such as air) can be used to pressurize the mixture, and the partial pressure of oxygen typically ranges between 0.38 MPa and 1.48 MPa.

An additive of the present invention is an aqueous sodium silicate solution. Any commercially available aqueous sodium silicate solution may be used, although it is preferable to use as pure of a sodium silicate solution as is practically possible. The sodium silicate solution may be added in an amount to achieve a concentration of from about 0.14% to about 1.4% SiO<sub>2</sub> on pulp. Preferably, the sodium silicate solution is added in an amount to achieve a concentration of from about 0.28% to about 1.12% SiO<sub>2</sub> on pulp.

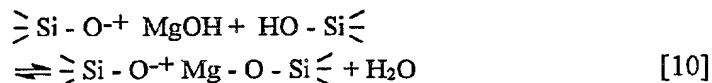
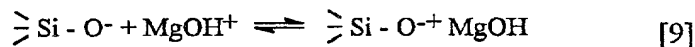
Another additive according to the present invention is a magnesium compound which dissociates in the solution to form Mg(OH)<sup>+</sup> cations. The magnesium compound should be added in an amount to achieve, along with any other dissociated magnesium, an Mg:SiO<sub>2</sub> mass ratio of between about 1:46 to

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about 1:2. Preferably, the Mg:SiO<sub>2</sub> mass ratio is between about 1:15 to about 1:3. Most preferably, the Mg:SiO<sub>2</sub> mass ratio is between about 1:10 to about 1:3. The mass ratio is of the total magnesium available for formation into Mg(OH)<sup>+</sup>, including any of the magnesium added and any magnesium inherent in the pulp and existing in a form which readily dissociates and forms Mg(OH)<sup>+</sup> over a pH range of at least 8:

The magnesium compound is added in an amount to achieve an actual concentration of from about 0.01 % to about 0.2 % Mg on pulp (again including any other source of available magnesium). More preferably, the magnesium compound is added in an amount to achieve a concentration of from about 0.02 % to about 0.2 % Mg on pulp. Preferably, the magnesium compound is magnesium sulfate, added as MgSO<sub>4</sub> or MgSO<sub>4</sub>·7H<sub>2</sub>O. Alternatively, the magnesium compound is MgO, MgCl<sub>2</sub>, Mg(OH)<sub>2</sub> and/or MgNO<sub>3</sub>, among others. Any number of magnesium compounds can be used, as long as they readily form Mg(OH)<sup>+</sup> at pH values of at least 8 and are not detrimental to process equipment.

A critical step in the present invention is the formation of the hydrolyzed magnesium cation Mg(OH)<sup>+</sup>. It is believed that this cation neutralizes dissociated silanol groups and causes silicate polymerization, as summarized by the equations written below:



Another additive of the present invention is an alkali agent added in an amount sufficient to maintain a pH of the solution of at least about 8. At pH values of at least about 8, magnesium exists as Mg(OH)<sup>+</sup> in an amount sufficient to initiate reaction [9] above. More preferably, the alkali agent is selected and added in an amount sufficient to maintain the pH to a range of between 8 and 12. The alkali agent may be NaOH, Na<sub>2</sub>O, MgO, Mg(OH)<sub>2</sub>, K<sub>2</sub>O, KOH, CaO, and/or Ca(OH)<sub>2</sub>. Preferably, the non-calcium containing compounds are selected to minimize the formation of silicate scales. Such silicate scales can be detrimental to the quality of the paper product and must be removed periodically resulting in costly stoppages of the process. Because MgO and Mg(OH)<sub>2</sub> can serve two functions, namely that as the magnesium compound which readily forms

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Mg(OH)<sup>+</sup> and as an alkali agent, then the magnesium compound and alkali agent can be combined as one additive in some cases.

According to a method of the present invention, the pulp is brightened by mixing the pulp with hydrogen peroxide, an aqueous sodium silicate solution, an alkali agent added in an amount sufficient to maintain the pH of the solution at least about 8, and a magnesium compound which dissociates in the solution to form Mg(OH)<sup>+</sup> cations, wherein the magnesium compound is added in an amount to achieve, along with any other dissociated magnesium, an Mg:SiO<sub>2</sub> mass ratio of between about 1:15 to about 1:3. This mixture is then heated, which allows the mixture to react to cause a portion of the lignin to degrade (i.e., to break down into a more soluble form to be washed away). In the case where a hydrogen peroxide/oxygen stage is used, the mixture is also pressurized with oxygen, in a known manner. While continuously heated, the chemicals are mixed into the pulp slurry which is retained at an elevated temperature for a period of time sufficient to allow the degradation reactions of the lignin to occur. This typically is between 30 minutes and four hours, depending on the temperature and concentration of the additives in the pulp. Typically, the mixture is heated to a temperature of between about 90°C and about 130°C.

As mentioned above, the present invention relies on the formation of high molecular weight silicates to adsorb transition metals to avoid the decomposition of hydrogen peroxide by transition metals. Accordingly, the present invention can be characterized as a method for brightening pulp by forming a sodium silicate solution having a high percentage of high molecular weight silicates by mixing sodium silicate and a magnesium compound which dissociates in the solution to form Mg(OH)<sup>+</sup> cations. Then, the sodium silicate solution is added to the pulp to adsorb at least a portion of the transition metals of the pulp. Any increased amount of higher molecular weight silicates appears to improve the adsorption of transition metals, but it is preferable that the constituents are added such that the sodium silicate solution has at least 25% of the silicates with a molecular weight of at least 10,000 daltons.

It is not believed that the order of addition is important to the functioning of the present invention. Typically, the magnesium compound is Epsom salt (MgSO<sub>4</sub>·7H<sub>2</sub>O) and is either first dissolved in water or dissolved directly in a commercial aqueous sodium silicate solution. Then the alkali agent(s) is added followed by H<sub>2</sub>O<sub>2</sub>. The combination is then mixed into the pulp slurry.

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EXAMPLES

The following examples are included to more clearly demonstrate the overall nature of the invention. These examples are exemplary, not restrictive, of the invention.

## Example 1

A kraft pulp was delignified by the ODEop partial sequence and had a kappa number of 2.7 and a viscosity of 19.0 cp. The ODEop partial sequence is called elemental chlorine-free or ECF. The pulp had a low initial Mg content (<50 ppm). The pulp was P/O (P=H<sub>2</sub>O<sub>2</sub>; O=O<sub>2</sub>) bleached at 12% consistency and 110°C for 2 hours using reagent grade H<sub>2</sub>O<sub>2</sub>, NaOH and MgSO<sub>4</sub>·7H<sub>2</sub>O. A technical grade sodium silicate solution sold by Fisher Scientific, which contained some transition metals, was used. An H<sub>2</sub>O<sub>2</sub> charge of 1.5% by weight on pulp was used with 2.0-2.3% NaOH by weight on pulp. The initial O<sub>2</sub> pressure for all P/O experiments was 0.38 MPa.

A first series of experiments was run to determine the effect of magnesium sulfate addition on the brightening of this ECF pulp. Table 1 shows both percentage of the constituents in each sample added to the pulp (on a dry weight basis) and the brightness, yield, viscosity, and residual H<sub>2</sub>O<sub>2</sub>. Samples 1 through 4 have the same amount of silicate, sodium hydroxide, and hydrogen peroxide, while the amount of the magnesium compound (in this case, magnesium sulfate) increases from Samples 1 through 4. In all of the tables in the examples, "silicate" refers to the weight percent of a 41 Bé silicate solution (28.7% SiO<sub>2</sub>) that was added. For all examples, the brightness was determined in accordance with TAPPI Standard T452 om-92. In addition, the pulp yield is the mass of washed pulp from the P or P/O stage divided by the mass of the feed to the stage. The viscosity and residual hydrogen peroxide (given as a percentage of the initial dose) were determined by known methods, including TAPPI Standard T230 om-94 for viscosity and iodometric titration for residual H<sub>2</sub>O<sub>2</sub>.

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Table 1

Effect of Magnesium Sulfate Application on P/O Bleaching of  
First ECF Kraft Pulp

	Sample 1	Sample 2	Sample 3	Sample 4
Silicate, % on pulp	4.0	4.0	4.0	4.0
NaOH, % on pulp	2.3	2.3	2.3	2.3
H <sub>2</sub> O <sub>2</sub> , % on pulp	1.5	1.5	1.5	1.5
MgSO <sub>4</sub> ·7H <sub>2</sub> O % on pulp	0.0	0.25	0.5	0.75
SiO <sub>2</sub> , % on pulp	1.148	1.148	1.148	1.148
Mg, % on pulp	0.0	0.025	0.050	0.075
Mg:SiO <sub>2</sub> mass ratio	0	1:46	1:23	1:15
End pH	10.2	10.5	11.0	11.2
Brightness, %	79.8	84.0	84.2	85.3
Yield, %	97.2	97.7	98.1	98.2
Viscosity, cp	8.8	11.4	13.5	14.1
Residual H <sub>2</sub> O <sub>2</sub> , %				
30 Minutes	2	25	35	33
60 Minutes	0	15	22	30
120 Minutes	0	2	7	10

Table 1 shows that an MgSO<sub>4</sub>·7H<sub>2</sub>O charge of 0.25% on pulp (250 ppm Mg on pulp) increased brightness significantly, namely from 79.8% to 84.0%. Also, the brightness increased further when 0.50 and 0.75% MgSO<sub>4</sub>·7H<sub>2</sub>O was used. The interesting and totally novel result from Table 1 is the increase in pulp yield caused by the addition of magnesium sulfate. Kraft pulps can be dissolved in a solution of cupriethylenediamine, and the viscosity of the solution is an indicator of the degree of polymerization of the cellulose in the pulp. It can be seen that a higher charge of magnesium sulfate also resulted in higher viscosities (less depolymerization of cellulose during H<sub>2</sub>O<sub>2</sub> brightening). However, the lowest viscosity (no MgSO<sub>4</sub>·7H<sub>2</sub>O) corresponds to an average DP of 815. It is unlikely that cellulose molecules of such high DP would solubilize. Therefore, it appears that hemicelluloses were being dissolved. Most likely, the free radicals from H<sub>2</sub>O<sub>2</sub> decomposition were causing depolymerization of the hemicelluloses to a degree that resulted in their solubilization.

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## Example 2

A second ECF pulp sample was obtained from the same mill serving as the source of the pulp used in Example 1. It had a kappa number of 2.4 and a viscosity of 20.5 cp. The transition metal content of the first ECF pulp was not measured but the second pulp contained 6 ppm Mn, 8 ppm Fe, and 2 ppm Cu. These values were lowered to 0.3, 3.7 and 1.5 ppm, respectively, after treatment with Na<sub>2</sub>DTPA. Sample 2 was bleached at 100°C, while Samples 1, 3, and 4 were bleached at 110°. Table 2 varies the charge of sodium silicate, with Samples 1 and 2 having no silicate added, while Samples 3 and 4 have a 2.0 and 4.0 % charge, respectively.

Table 2  
Effect of Silicate on P/O Bleaching of Second ECF Kraft Pulp.  
Chelated Pulp: 0.3 ppm Mn, 3.7 ppm Fe and 1.5 ppm Cu

	Sample 1	Sample 2	Sample 3	Sample 4
Silicate, % on pulp	0.0	0.0	2.0	4.0
NaOH, % on pulp	2.0	2.0	2.0	2.0
H <sub>2</sub> O <sub>2</sub> , % on pulp	1.5	1.5	1.5	1.5
MgSO <sub>4</sub> · 7H <sub>2</sub> O % on pulp	0.5	0.5	1.0	0.5
SiO <sub>2</sub> , % on pulp	0.0	0.0	0.574	1.148
Mg, % on pulp	0.05	0.05	0.10	0.05
Mg:SiO <sub>2</sub> mass ratio	NA*	NA*	1:6	1:23
End pH	10.9	10.9	10.5	10.9
Brightness, %	85.1	84.3	85.7	85.3
Yield, %	98.0	98.3	98.2	98.6
Viscosity, cp	12.6	13.7	16.3	13.7
Residual H <sub>2</sub> O <sub>2</sub> , %				
30 Minutes	24.9	31.5	38.2	41.5
60 Minutes	10.0	19.9	28.2	31.5
120 Minutes	3.3	6.6	14.9	14.9

\*Not applicable

Table 2 shows slight increases in brightness and yield of the chelated sample when the amount of sodium silicate is increased. The low transition metal contents of this pulp, particularly the 0.3 ppm Mn, can be achieved in only a few commercial installations. More significantly, the presence of sodium silicate

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shows a significant increase in residual hydrogen peroxide, which is important in maintaining brightness. In the absence of silicate, the  $H_2O_2$  residual for most pulp samples would be zero after two hours at 110°C.

### Example 3

Four more samples of the same ECF pulp used in Example 2, having a kappa number of 2.4 and a viscosity of 20.5 cp, were tested. In this case, the pulp was unchelated. In Samples 1 and 2 below, the temperature of the stage was 90°C while the temperature of Samples 3 and 4 was 110°C. Samples 1 and 3 contained no silicate, while Samples 2 and 4 did.

Table 3  
Effect of Temperature on P/O Bleaching of Second ECF Kraft Pulp.  
Unchelated Pulp: 6 ppm Mn, 8 ppm Fe and 2 ppm Cu

	Sample 1	Sample 2	Sample 3	Sample 4
Temperature, °C	90	90	110	110
Silicate, % on pulp	0	2.0	0	2.0
NaOH, % on pulp	2.0	2.0	2.0	2.0
$H_2O_2$ , % on pulp	1.5	1.5	1.5	1.5
$MgSO_4 \cdot 7H_2O$ % on pulp	0.5	1.0	0.5	1.0
$SiO_2$ , % on pulp	0.0	0.574	0.0	0.574
Mg, % on pulp	0.05	0.1	0.05	0.1
Mg: $SiO_2$ mass ratio	NA	1:6	NA	1:6
End pH	11.3	11.6	9.9	10.9
Brightness, %	78.0	79.9	79.7	81.8
Yield, %	98.5	98.7	97.9	98.5
Viscosity, cp	15.4	15.7	11.5	14.1
Residual $H_2O_2$ , %				
30 Minutes	3.3	18.2	1.7	10.0
60 Minutes	1.7	10.0	0.0	5.0
120 Minutes	0.0	5.0	0.0	3.3

Table 3 shows that, at either temperature, the inclusion of sodium silicate improves the brightening process. At 90°C, a sample having sodium silicate gave no noticeable improvement in yield but 1.9% increase in brightness. At 110°C, a sample including sodium silicate caused a 0.6% increase in yield and a 2.1% increase in brightness. Also, as before, the presence of sodium silicate



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showed a significant increase in residual hydrogen peroxide, which is important in maintaining brightness.

#### Example 4

Bleached and unbleached samples of de-inked, mixed office waste (MOW) consisting of 65% sorted white ledger and 35% office pack were obtained from a mill in the American Midwest. This pulp sample was from almost exclusively chemical pulps. The properties of the samples are summarized in Table 4. High positive b\* value indicates a yellowish tint and a high negative value indicates a bluish tint. A high positive a\* value indicates a reddish tint and a high negative value indicates a greenish tint. The aim of bleaching is to decrease the absolute a\* and b\* values to as close to zero and increase the L\* value as high as possible. As shown in Table 4, the effect of the addition of silicate and magnesium sulfate to MOW was determined.

Table 4  
Effect of Silicate Addition on P/O Bleaching of Mixed Office Waste (MOW)

Pulp <sup>1</sup>	MOW	MOW	BL. MOW	BL. MOW
Silicate, % on pulp	0.0	4.0	0.0	4.0
NaOH, % on pulp	2.3	2.3	2.3	2.3
H <sub>2</sub> O <sub>2</sub> , % on pulp	1.5	1.5	1.5	1.5
MgSO <sub>4</sub> ·7H <sub>2</sub> O on pulp	0.5	0.5	0.5	0.5
SiO <sub>2</sub> , % on pulp	0.0	1.148	0.0	1.148
Mg, % on pulp	0.05	0.05	0.05	0.05
Mg:SiO <sub>2</sub> mass ratio	NA	1:23	NA	1:23
End pH	10.1	10.2	10.0	10.0
Brightness, %	77.9	80.4	85.4	88.3
L*	91.51	91.86	94.79	95.24
a*	-0.46	0.22	0.27	-0.07
b*	1.67	0.73	1.68	0.48
Yield, %	95.4	96.5	97.3	97.4
Viscosity, cp	9.8	11.0	9.7	11.1
Residual H <sub>2</sub> O <sub>2</sub> , % of Applied				
30 Minutes	2	27	3	28
60 Minutes	0	10	1	15
120 Minutes	0	5	0	7

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<sup>1</sup>Mixed office waste (MOW) pretreated with 0.2% DTPA: Brightness, 74.2;  $L^*=89.78$ ;  $a^*=0.76$ ;  $b^*=1.77$ . Commercially bleached mixed office waste (BLMOW) pretreated with 0.2% DTPA: Brightness, 83.6,  $L^*=94.4$ ;  $a^*=0.28$ ;  $b^*=1.72$ .

5 It can be seen (footnotes of Table 4) that  $H_2O_2$  bleaching in the mill ( $\sim 1.0\%$   $H_2O_2$ ,  $\sim 95^\circ C$ ) did not significantly lower the  $b^*$  value. Both the unbleached and commercially bleached samples were treated with  $Na_2DTPA$  then brightened with  $1.5\%$   $H_2O_2$  at  $110^\circ C$ . For the unbleached sample, the inclusion of  $4.0\%$  silicate resulted in an improvement of 2.5 brightness points. The  $a^*$  and  $b^*$  values were closer to zero as well. Similar benefits were obtained when the  
10 commercially bleached pulp was brightened further. Without silicate, no significant decrease in  $b^*$  was obtained. A high temperature and high  $H_2O_2$  residuals apparently are required to destroy the colored contaminants responsible for the  $b^*$  value. The inclusion of silicate increased the yield of the unbleached  
15 pulp by  $1.1\%$ .

#### Example 5

The results in Table 1 showed increased brightness with an increase in the dose ratio of  $MgSO_4 \cdot 7H_2O$ :sodium silicate (41 Bé). The dose ratio was increased further in Table 2 where  $2\%$  sodium silicate and  $1.0\%$   $MgSO_4 \cdot 7H_2O$  on  
20 pulp were used (i.e., Sample 3 of Table 2), which resulted in the highest brightness ( $85.7\%$ ) for the ECF pulps. In this Example, the effect of dose ratio on the brightening of a totally chlorine-free (TCF) pulp is investigated.

The TCF pulp (kraft) was from a Swedish mill and it had a kappa number of 7.4 and a viscosity of 23.4 cp. It also contained 1.9 ppm Mn, 4.7 ppm  
25 Fe, and 0.8 ppm Cu. After it was acid-washed it contained 0.1 ppm Mn, 4.0 ppm Fe, and 0.8 ppm Cu. The acid-washed pulp was brightened with various dose ratios of  $MgSO_4 \cdot 7H_2O$ :sodium silicate. The  $H_2O_2$  and NaOH charges were  $2.0\%$  and  $2.5\%$  on pulp, respectively, and the pulps were brightened for two hours at  $110^\circ C$  and  $12\%$  consistency.

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Table 5  
Effect of Silicate and  $MgSO_4 \cdot 7H_2O$  on  
P/O Bleaching of Acid-Washed TCF Pulps

	Sample 1	Sample 2	Sample 3	Sample 4
Silicate, % on pulp	0	4.0	2.0	1.0
NaOH, % on pulp	2.5	2.5	2.5	2.5
$H_2O_2$ , % on pulp	2.0	2.0	2.0	2.0

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	Sample 1	Sample 2	Sample 3	Sample 4
MgSO <sub>4</sub> ·7H <sub>2</sub> O % on pulp	0.5	0.5	1.0	1.0
SiO <sub>2</sub> , % on pulp	0	1.148	0.574	0.287
Mg, % on pulp	0.05	0.05	0.10	0.10
Mg:SiO <sub>2</sub> mass ratio	NA	1:23	1:6	1:3
End pH	10.5	11.3	10.9	10.8
Brightness, %	75.4	78.2	79.4	77.9
Yield, %	96.3	98.2	98.3	98.0
Viscosity, cp	9.1	13.1	15.5	12.8
Residual H <sub>2</sub> O <sub>2</sub> , %				
30 Minutes	15	32	37	31
60 Minutes	4	19	16	8
120 Minutes	0	5	5	1

The brightness and yield were relatively low when silicate was excluded (Sample 1 of Table 5). The highest brightness was obtained with MgSO<sub>4</sub>·7H<sub>2</sub>O:sodium silicate dose ratio of 1%:2%. The next highest brightness was for dose ratio 0.5%:4%, followed by 1%:1%.

5 A general trend from the first five tables is that, for a given temperature, higher brightness and yields are obtained as H<sub>2</sub>O<sub>2</sub> stabilization is improved (higher residuals). There is not an exact correlation because, for these experiments, the accuracy on H<sub>2</sub>O<sub>2</sub> residual was about  $\pm 5\%$  of the initial charge. However, final brightness in Table 5 correlates with H<sub>2</sub>O<sub>2</sub> residual after 30  
10 minutes.

The three dose ratios in Table 5, i.e. 0.5:4.0; 1.0:2.0; and 1.0:1.0, were used in a pulp-free system to deactivate 1 ppm, each Mn<sup>2+</sup>, Fe<sup>3+</sup>, and Cu<sup>2+</sup> added simultaneously to the alkaline solution. For each dose ratio, the initial solution phase concentrations of H<sub>2</sub>O<sub>2</sub>, MgSO<sub>4</sub>·7H<sub>2</sub>O, and sodium silicate were  
15 identical to when pulp was present. In the absence of pulp, less NaOH was required to achieve pH 11.2 taken as a rough average for P/O bleaching. The solutions were retained at 110°C for two hours then cooled and ultra-filtration was used to separate high and low molecular weight silicates. Membranes with 10,000 MW cutoff were used.

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The results will be analyzed in terms of ppm Si in solution. The 41 Bé silicate solution that was used contained 28.7% SiO<sub>2</sub>. Therefore 4% silicate on pulp corresponds to 1.148 SiO<sub>2</sub> on pulp or 0.536% Si on pulp. One hundred grams of pulp at 12% consistency is associated with 733 mL of solution (assuming a specific gravity of 1.0). Therefore, the Si concentration is 0.536 g in 733 mL or 0.731 g/L (~730 ppm). The solutions passing through the membrane were analyzed for Si, Mn, Fe and Cu concentrations by ICP spectroscopy. The results are presented in Table 6.

Table 6

Mg and Silicate Conc., ppm in Solution	Conc. Passing Through Membrane			
	Si	Mn	Fe	Cu
68 ppm Mg* + 730 ppm Si	617	0.008	0.023	0.027
136 ppm Mg + 365 ppm Si	194	0.001	0.001	0.016
136 ppm Mg + 183 ppm Si	56	0.004	0.001	0.018

\*0.5% MgSO<sub>4</sub> · 7H<sub>2</sub>O on pulp

Table 6 shows that in the case of 0.5% MgSO<sub>4</sub>·7H<sub>2</sub>O and 4% silicate, 85% of the Si passes through the membrane as low molecular weight compounds. However, less than 3% of the Fe and Cu and less than 1% of the Mn pass through. The transition metals appear to be bound to the high molecular weight silicate retained on the membrane. The data would suggest that 1.0% MgSO<sub>4</sub>·7H<sub>2</sub>O and 2.0% silicate give the best transition metal deactivation, particularly of Mn which is believed to be the most aggressive catalyst for H<sub>2</sub>O<sub>2</sub> decomposition. The significance of the differences between 1, 4, and 8 ppb Mn or 16, 18 and 27 ppb Cu in solution might be deemed insignificant. However, there is no doubt that it is the high molecular weight silicate that adsorbs or complexes the transition metals. The amount of high molecular weight silicate (greater than 10,000 daltons) for the various formulations are 113 ppm Si for 0.5%:4.0%; 127 ppm for 1.0%:1.0%; and 171 ppm for 1.0%:2.0%. The clear superiority of the 1%:2.0% formulation in Table 6 is now evident.

#### Example 6

The ECF pulp of Example 1 used for peroxide/oxygen bleaching was treated with an acidic chlorine dioxide stage while the TCF pulp was acid-washed. Calcium that was bound to the pulps dissolved in the acidic solutions and was washed out. Six effluents from peroxide/oxygen bleaching of ECF pulps and

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five effluents from TCF pulps were collected and divided in two. Calcium chloride was added to one half of each effluent to give a concentration of 50 ppm  $\text{Ca}^{2+}$  in solution. Smaller volumes of the straight and calcium-enriched effluents were adjusted to pH values of 9.0 and 10.0, than one inch square strips of 20-mesh stainless steel were placed in each solution or slurry. All of the selected effluents contained both epsom salt and sodium silicate. There was no magnesium silicate precipitate at either pH value, but there were calcium-magnesium silicate precipitates in most of the eleven effluents that were enriched with calcium chloride.

Each metal strip weighed about 1.6 grams initially and, surprisingly, none of them gained any weight when placed in any of the magnesium silicate solutions or the calcium-magnesium silicate slurries for more than 96 hours at room temperature (about 20°C). When taken from the solution or slurry, each strip weighed within 2 milligrams of its initial weight after washing and air-drying. This confirms that calcium silicates adhere to metals while calcium-magnesium and magnesium silicates do not.

Unbleached pulps are normally not acid-washed or treated with chelating-agents before  $\text{O}_2$  delignification. Therefore, pulps normally enter an oxygen delignification stage with higher concentrations of calcium than that of pulps entering a peroxide/oxygen stage. However, if 1% epsom salt and 2% sodium silicate is added, there would be enough magnesium cations to chemisorb most of the dissociated silanol groups at pH values less than 11. Since magnesium cations are preferentially chemisorbed over calcium cations, any potential precipitate would be rich in magnesium. It is unlikely that such precipitates would scale the oxygen washers, where the pulp is washed after oxygen delignification. Scaling is unlikely at the high pH values of the black liquor (i.e., washed liquor from the unbleached pulp) evaporators, which are used to evaporate moisture after washing and before burning the now concentrated black liquor in a kraft recovery furnace. The likely scenario is that the calcium-magnesium silicate will pass through the kraft recovery furnace and be removed with the dregs at the green liquor clarifier. (Green liquor is the viscous fluid removed from the bottom of the recovery furnace and is made up primarily of inorganic compounds, such as sodium sulfide and sodium carbonate.) After removal, green liquor is diluted and insoluble materials (i.e., dregs) are separated by sedimentation. A high rate of sedimentation is observed for these calcium-magnesium silicate particles.

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The effect of the magnesium sulfate/sodium silicate combination on oxygen delignification is demonstrated below in Table 7. Two-stage oxygen delignification of a 41 kappa number kraft pulp was simulated by adding 2% NaOH on pulp and 0.72 MPa of oxygen at 12% consistency and 90°C for 30 minutes, followed by a second NaOH injection (1.0% NaOH on pulp), restoration of oxygen pressure, and 30 minutes of additional retention. The standard oxygen included 0.5% epsom salt on pulp added during the preheat stage, i.e., before all other chemicals. When silicate was used, 1% Epsom salt on pulp was added at the preheat stage and 2% sodium silicate was added along with the first sodium hydroxide injection. Silicate additions significantly improved delignification selectivity (kappa number versus viscosity). Pulp brightness is also increased.

Table 7

Effect of Silicate Addition on Kappa Number and Viscosity After O<sub>2</sub> Delignification

	Standard Oxygen	O <sub>2</sub> with Silicate
MgSO <sub>4</sub> 7H <sub>2</sub> O, % on pulp	0.5	1.0
Silicate, % on pulp	0	2.0
end pH	11.0	11.6
Brightness, %	28.2	30.8
Kappa No.	20.4	20.0
Viscosity, cP	21.2	24.7

<sup>1</sup>Laboratory pulp made from 5 kg of chips, kappa number 41, viscosity 35 cP and screened yield of 47.8%

The improvement in viscosity is significant because viscosity is lowered further by most delignification and brightening stages, including P/O stages. If the viscosity is lowered below 10-12 cP (DP ~ 1000) then the strength values of paper made from the pulp decline dramatically.

Although illustrated and described herein with reference to certain specific embodiments and examples, the present invention is nevertheless not intended to be limited to the details shown. Rather, the claims should be read to include various modifications within the scope and range of equivalents of the claims, without departing from the spirit of the invention.

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What is Claimed is:

- 1                   1.     A combination of additives for use in a brightening stage of  
2     pulps containing less than 18% lignin, said combination comprising: an aqueous  
3     sodium silicate solution; an alkali agent added in an amount sufficient to maintain  
4     a pH of said solution at least about 8; and a magnesium compound which  
5     dissociates in said solution to form  $\text{Mg}(\text{OH})^+$  cations, wherein said magnesium  
6     compound is added in an amount to achieve, along with any other dissociated  
7     magnesium, an  $\text{Mg}:\text{SiO}_2$  mass ratio of between about 1:46 to about 1:2.
- 1                   2.     A combination of additives in accordance with claim 1,  
2     wherein said  $\text{Mg}:\text{SiO}_2$  mass ratio is between about 1:15 to about 1:3.
- 1                   3.     A combination of additives in accordance with claim 1,  
2     wherein said alkali agent is added in an amount sufficient to maintain the pH of  
3     said solution within the range of from about 8 to about 12.
- 1                   4.     A combination of additives in accordance with claim 1,  
2     wherein said magnesium compound is magnesium sulfate, added as  $\text{MgSO}_4$  or  
3      $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$ .
- 1                   5.     A combination of additives in accordance with claim 1,  
2     wherein:  
3                   said aqueous sodium silicate solution is added in an amount to  
4     achieve a concentration of from about 0.14% to about 1.4%  $\text{SiO}_2$  on pulp; and  
5                   said magnesium compound is added in an amount to achieve a  
6     concentration of from about 0.01% to about 0.2% Mg on pulp.
- 1                   6.     A combination of additives in accordance with claim 5,  
2     wherein:  
3                   said aqueous sodium silicate solution is added in an amount to  
4     achieve a concentration of from about 0.28% to about 1.12%  $\text{SiO}_2$  on pulp; and  
5                   said magnesium compound is added in an amount to achieve a  
6     concentration of from about 0.02% to about 0.2% Mg on pulp.

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1           7.     A combination of additives in accordance with claim 1,  
2     wherein said alkali agent is selected from the group consisting of at least one of  
3     NaOH, Na<sub>2</sub>O, MgO, Mg(OH)<sub>2</sub>, K<sub>2</sub>O, KOH, CaO, and Ca(OH)<sub>2</sub>.

1           8.     A combination of additives in accordance with claim 1,  
2     wherein said magnesium compound is selected from the group consisting of at  
3     least one of MgO, MgCl<sub>2</sub>, Mg(OH)<sub>2</sub> and MgNO<sub>3</sub>.

1           9.     An aqueous composition for use in a brightening stage of  
2     pulps comprising:

3                 pulp containing less than 18% lignin;

4                 an aqueous sodium silicate solution;

5                 an alkali agent added in an amount sufficient to maintain the pH at  
6     least about 8; and

7                 a magnesium compound which dissociates in said solution to form  
8     Mg(OH)<sup>+</sup> cations, wherein said magnesium compound is added in an amount to  
9     achieve, along with any other dissociated magnesium, an Mg:SiO<sub>2</sub> mass ratio of  
10    between about 1:46 to about 1:2.

1           10.    An aqueous composition in accordance with claim 9, wherein  
2     said Mg:SiO<sub>2</sub> mass ratio is between about 1:15 to about 1:3.

1           11.    An aqueous composition in accordance with claim 9, wherein  
2     said alkali agent is added in an amount sufficient to maintain the pH of said  
3     solution within the range of from about 8 to about 12.

1           12.    An aqueous composition in accordance with claim 9, wherein  
2     said magnesium compound is magnesium sulfate, added as MgSO<sub>4</sub> or  
3     MgSO<sub>4</sub>·7H<sub>2</sub>O.

1           13.    An aqueous composition in accordance with claim 9, wherein:  
2                 said aqueous sodium silicate solution is added in an amount to  
3     achieve a concentration of from about 0.14% to about 1.4% SiO<sub>2</sub> on pulp; and

4                 said magnesium compound is added in an amount to achieve a  
5     concentration of from about 0.01% to about 0.2% Mg on pulp.

1           14.    An aqueous composition in accordance with claim 13,  
2     wherein:



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3           said aqueous sodium silicate solution is added in an amount to  
4 achieve a concentration of from about 0.28% to about 1.12% SiO<sub>2</sub> on pulp; and

5           said magnesium compound is added in an amount to achieve a  
6 concentration of from about 0.02% to about 0.2% Mg on pulp.

1           15. An aqueous composition in accordance with claim 9, wherein  
2 said alkali agent is selected from the group consisting of at least one of NaOH,  
3 Na<sub>2</sub>O, MgO, Mg(OH)<sub>2</sub>, K<sub>2</sub>O, KOH, CaO and Ca(OH)<sub>2</sub>.

1           16. An aqueous composition in accordance with claim 9, wherein  
2 said magnesium compound is selected from the group consisting of at least one of  
3 MgO, MgCl<sub>2</sub>, Mg(OH)<sub>2</sub> and MgNO<sub>3</sub>.

1           17. An aqueous composition in accordance with claim 9, wherein  
2 said pulp contains less than 5% lignin.

1           18. An aqueous composition in accordance with claim 17,  
2 wherein said pulp contains less than 2% lignin.

1           19. An aqueous composition in accordance with claim 9 further  
2 comprising hydrogen peroxide.

1           20. A method for brightening pulp comprising the steps of:  
2           mixing pulp containing less than 18% lignin with hydrogen  
3 peroxide, an aqueous sodium silicate solution; an alkali agent added in an amount  
4 sufficient to maintain the pH of said solution at least about 8; and a magnesium  
5 compound which dissociates in said solution to form Mg(OH)<sup>+</sup> cations, wherein  
6 said magnesium compound is added in an amount to achieve, along with any other  
7 dissociated magnesium, an Mg:SiO<sub>2</sub> mass ratio of between about 1:46 to about  
8 1:2, to form a mixture; and

9           heating said mixture to allow said mixture to react to cause a portion  
10 of said lignin to degrade.

1           21. A method in accordance with claim 20 further comprising  
2 pressurizing said mixture with an oxygen-containing gas.

1           22. A method for delignifying and brightening pulp comprising  
2 the steps of:

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3 mixing pulp containing less than 18% lignin with an aqueous sodium  
4 silicate solution; an alkali agent added in an amount sufficient to maintain the pH  
5 of said solution at least about 8; and a magnesium compound which dissociates in  
6 said solution to form  $\text{Mg}(\text{OH})^+$  cations, wherein said magnesium compound is  
7 added in an amount to achieve, along with any other dissociated magnesium, an  
8  $\text{Mg}:\text{SiO}_2$  mass ratio of between about 1:46 to about 1:2, to form a mixture;

9 pressurizing said mixture with an oxygen-containing gas; and  
10 heating said mixture to allow said mixture to react to cause a portion  
11 of said lignin to degrade.

1 23. A method in accordance with claim 22 wherein the oxygen  
2 partial pressure is in the range of between about 0.38 to about 1.48 MPa.

1 24. A method for brightening pulp containing transition metals  
2 and less than 18% lignin, said method comprising the steps of:

3 forming a sodium silicate solution having a high percentage of high  
4 molecular weight silicates by mixing sodium silicate and a magnesium compound  
5 which dissociates in said solution to form  $\text{Mg}(\text{OH})^+$  cations; and

6 adding said sodium silicate mixture to said pulp to adsorb at least a  
7 portion of said transition metals.

1 25. A method of claim 24, wherein said sodium silicate mixture  
2 has at least 25% of the silicates with molecular weight of at least 10,000 daltons.

# Declaration and Power of Attorney For Patent Application

## English Language Declaration

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name,

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled  
PEROXIDE, OXYGEN, AND PEROXIDE/OXYGEN BRIGHTENING OF CHEMICAL AND MIXED WASTE PULPS,

the specification of which is attached hereto unless the following box is checked:



was filed on 15 May 1998 as

United States Application Number or PCT International Application Number PCT/US98/10070  
 and was amended on 16 August 2000 (if applicable).

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR § 1.56.

I hereby claim foreign priority benefits under 35 U.S.C. §119(a)-(d) or § 365(b) of any foreign application(s) for patent or inventor's certificate, or § 365(a) of any PCT International application which designated at least one country other than the United States, listed below and have also identified below by checking the box, any foreign application for patent or inventor's certificate, or PCT International application having a filing date before that of the application on which priority is claimed:

Prior Foreign Application(s)

Priority Not Claimed

_____	_____	_____	<input type="checkbox"/>
(Number)	(Country)	(Day/Month/Year Filed)	
_____	_____	_____	<input type="checkbox"/>
(Number)	(Country)	(Day/Month/Year Filed)	

I hereby claim the benefit under 35 U.S.C. § 119(e) of any United States provisional application(s) listed below.

_____	_____
(Application Number)	(Filing Date)
_____	_____
(Application Number)	(Filing Date)

I hereby claim the benefit under 35 U.S.C. § 120 of any United States application(s), or 365(c) of any PCT International application designating the United States, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT International application in the manner provided by the first paragraph of 35 U.S.C. § 112, I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR § 1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application:

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Prior Foreign Application(s)

Priority Not Claimed

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(Number)

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(Country)

\_\_\_\_\_  
(Day/Month/Year Filed)

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(Application Number)

(Filing Date)

(Status - patented, pending, abandoned)

(Application Number)

(Filing Date)

(Status - patented, pending, abandoned)

POWER OF ATTORNEY: As a named inventor, I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and transact all business in the Patent and Trademark Office connected therewith:

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Andrew L. Ney	Reg. No. 20,300	Robert L. Andersen	Reg. No. 25,771	Christopher I. Halliday	Reg. No. 42,621
Kenneth N. Nigon	Reg. No. 31,549	Joshua L. Cohen	Reg. No. 38,040	Scott A. Mckeown	Reg. No. 42,866
Kevin R. Casey	Reg. No. 32,117	Daniel N. Calder	Reg. No. 27,424		
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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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(Application Number)

(Filing Date)

(Status - patented, pending, abandoned)

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(Filing Date)

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Additional inventors are being named on separately numbered sheets attached hereto.